

Druckminderventil, federbelastet Pressure-Reducing-Valve, springloaded

für Dämpfe, Gase und Flüssigkeiten, für sehr kleinen Minderdruck
for steam, gases and liquids, for very low reduced pressure

Typ 74

Discharge capacities for saturated steam

for definition the size of Pressure-Reducing-Valve

Size		0	I		II		III		III B	
Over- pressure p_0 [bar(g)]	Nominal pipe	10	15	20	25	32	40	50	50	65
		3/8	1/2	3/4	1	1 1/4	1 1/2	2	2	2 1/2
		kg/h								
$t_{\max}$ 200 °C	0,15	4	10	17	27	40	83	120	120	180
	0,2	5	11	19	31	46	99	145	145	210
	0,3	6	13	23	35	55	112	160	160	240
	0,5	7	16	28	46	70	140	200	200	300
	0,75	9	20	35	57	85	175	250	250	370
	1	11	25	42	68	100	210	300	300	450
	1,5	14	32	55	90	140	280	400	400	590
	2	17	40	70	115	170	350	520	520	750
	2,5	21	47	84	135	200	400	600	600	880
	3	24	55	99	155	240	480	700	700	1020
	4	31	70	123	195	300	600	890	890	1300
	5	38	85	150	245	360	740	1080	1080	1600
	6	46	104	185	300	450	900	1340	1340	1950
	7	54	122	225	350	540	1100	1600	1600	2400
	8	62	140	250	400	600	1250	1800	1800	2700

- a) To the definition of the right valve size according to the table, the downstream pressure is considerably. The usual piping speeds are appropriate for the table codes.
- b) The valve size determined under a) can be selected around a nominal size smaller, if it is noted that the pipe diameter at the valve outlet is increased around at least one nominal size.

Gaskets for steam:

$P_1 < 4$ [bar(g)] (<150°C): Piston gasket PTFE
Gasket ring EPDM

$P_1 < 15$ [bar(g)] (<200°C): Piston gasket PTFE
Gasket ring AF 100

To small pressure ratios applies:

$$\begin{aligned} \text{absolute reduced pressure } p \text{ [bar]} & \geq 0,7 \Rightarrow \text{correction factor} = 1,25 \\ \text{absolute inlet pressure } p \text{ [bar]} & \geq 0,8 \Rightarrow \text{correction factor} = 1,60 \\ & \geq 0,9 \Rightarrow \text{correction factor} = 2,25 \end{aligned}$$

$$\dot{m}_D = \dot{m}_D^1 \cdot f$$

The found correction factor must be multiplied due to the smaller flow rate by the given mass flow. With the help of the calculated value now a valve can be determined in accordance with the table.

With smaller pressure ratios than 0.7 no correction factor is used.

For superheated steam:

$$\dot{m}_D = \frac{V_H}{V_S} \cdot \dot{m}_D^1 \cdot f$$

* V_H : specific volume of the superheated steam

* V_S : specific volume of the saturated steam

f : correction factor

$\dot{m}_D^1$: given mass flow

$\dot{m}_D$: resulting value of the mass flow, with that the table can be used.

* see VDI Steam table

If the downstream pipe should be longer than 3 meters, then it is to be selected around one nominal size stage more largely.

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